

Mass Balance

Lecture Note
Principles of Food Engineering

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Mass Balance Learning Objectives

- Understand the fundamental mass balance concepts
- Be able to list and discuss important mass balance applications in food processing and handling operations
- Be able to conceptually describe how mass balance determinations or calculations are obtained

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WHY STUDY MASS BALANCE???

- Fundamental for blending of ingredients in food processing operations
- Fundamental for separation processes include:
 - evaporation
 - dehydration
 - distillation
 - absorption
 - ion exchange

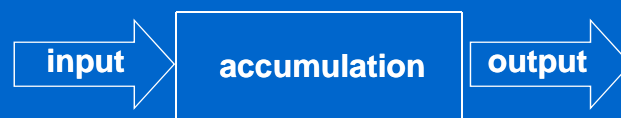
Law of conservation of mass :
Matter is neither be created nor destroyed

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Mass Balance : Concept 1

- Law of Conservation of Mass

$$\text{Input} - \text{output} = \text{accumulation}$$



- Continuous/steady state processes :
 - No accumulation of mass
- Desired in large-scale operations :
 - process control : simpler
 - product quality : easier to manage
- In small scale operations, batch processing of ingredients is more common
- Combination of continuous and batch type operations sometimes used

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Mass Balance : Concept 2

Yield concept

- Grinding of soybean
 - Results : 93 kg soy flour are produced from 100 kg soybean
Yield : 93%.
- (Bio)chemical reaction : Yield concept----> stoichiometry
 - ex. $C_6H_4(CH_3)_2 + 3O_2 \rightarrow C_6H_4(CO)_2O + 3 H_2O$
xylene (X) phthalic anhydride (Ph)
 - Results : 108 kg of Ph are produced per 100 kg X
Yield??

MW X = 106 kg/kg mole

MW Ph = 148 kg/kg mole

100 kg X = 100 kg(1 kg mole/106 kg) = 0.944 kg mole

108 kg Ph = 108 kg(1kg mole/148 kg) = 0.730 kg mole

Yield : $(0.730/0.944)100\% = 77.3\%$

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Steps in Mass Balance Preparation

- Draw a sketch or diagram describing process
 - Identify information available
- Identify boundaries of system with dotted lines
 - Identify all input (inflows) and output (outflows)
- Use symbols or letters to identify unknown items/quantities
- Write mass balance equation :
 - choose appropriate basis of calculation
 - do total and/or component mass balance
- Solve resulting algebraic equation(s)

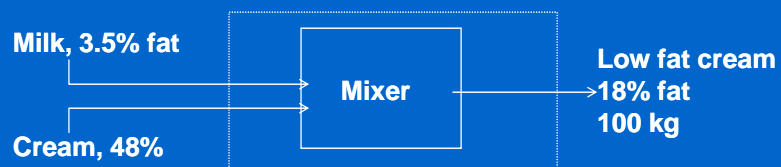
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Mass Balance Example 0

Production of low fat cream (18% fat, w/w), from double cream (48% fat, w/w) and milk (3.5%,w/w).
Howmuch double cream and milk are required to produce 100 kg low fat cream?

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Mass Balance Example 0answer



Let the required double cream = y kg and milk = x kg

Total mass balance equation :

$$y + x = 100 \text{ kg} \quad \text{..... Eq.1}$$

The componen balance on the fat :

$$0.035x + 0.48y = 100(0.18) \quad \text{..... Eq.2}$$

Eq. 1 and 2 :

$$0.035(100-y) + 0.48y = 18$$

$$3.5 - 0.035y + 0.48y = 18$$

$$y = 32.58 \text{ kg}$$

$$X = 67.42 \text{ kg}$$

jadi

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Mass Balance Example 1

- Drying of 500 kg/h of diced carrots
- Dryer used : parallel-flow dehydrator
- Drying objective : moisture content 85% to 20%
- Air entering dehydrator
 - air humidity ratio of 0.013 kg of water per kg of dry matter entering dehydrator at the rate of 200 kg of air per kg of dry solid
- Calculate humidity ratio of the air leaving dehydrator

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Mass Balance Example 1 Answer (i)

Step 1. Draw a sketch or diagram describing process



Step 2. Identify boundaries of system with dotted lines

Step 3. Use symbols or letters to identify unknown items/quantities

- Let m represent total water contained in 1 kg dry leaving air

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Mass Balance Example 1 Answer (ii)

Step 4. Write mass balance equation



Balance of water :
Total of water in = total of water out

$$(\text{H}_2\text{O carrots} + \text{H}_2\text{O air})_{\text{in}} = (\text{H}_2\text{O carrots} + m)_{\text{out}}$$

Basis : 1 kg dry basis

$(\text{H}_2\text{O carrots})_{\text{in}}$: 85 parts of H_2O 15 part of dry solids
for 1 kg of dry solids : $1.0(85/15) = 5.67 \text{ kg H}_2\text{O}$

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Mass Balance Example 1 Answer (iii)

Step 4. Write mass balance equation



$(\text{H}_2\text{O air})_{\text{in}}$: for 1 kg of dry solids > 200 kg of dry air

$$\frac{(200) \text{ kg dry air}}{\text{kg dry solids}} \times \frac{(0.013) \text{ kg water}}{\text{kg dry air}} = 2.6 \text{ kg H}_2\text{O}$$

$(\text{H}_2\text{O carrots})_{\text{out}}$: $1.0(20/80) = 0.25 \text{ kg H}_2\text{O}$

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Mass Balance Example 1 Answer (iv)



Water balance equation :

$$\frac{5.67 \text{ kg water}}{\text{kg dry solids}} + \frac{2.6 \text{ kg of water}}{\text{kg dry solids}} = \frac{0.25 \text{ kg of water}}{\text{kg dry solids}} + m$$

$$5.67 + 2.6 = 0.25 + m$$

Step 5. Solve resulting algebraic equation

$$m = 5.67 + 2.6 - 0.25 = \frac{8.02 \text{ kg water}}{\text{kg dry solids}}$$

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Mass Balance Example 1 Answer (v)



humidity ratio, $W_2 =$

..... Moisture content of air leaving dehydrator

$$\frac{8.02 \text{ kg water}}{200 \text{ kg dry solids}} = \frac{8.02 \text{ kg water} / \text{kg solids}}{200 \text{ kg dry/kg solids}} = \frac{0.04 \text{ kg water}}{\text{kg dry air}}$$

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Contoh Soal Neraca Massa2

- Contoh- proses pencampuran sirup sorgum
- Pencampuran sirup murni dengan sirup jagung dan sirup-semi untuk memperoleh 100 kg “blended product”

- Berikut adalah karakteristik 3 macam sirup :

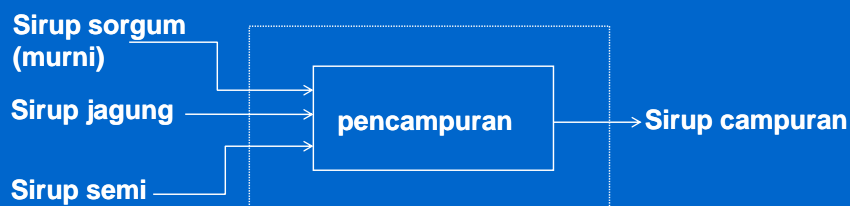
Item	%H ₂ O	%gula	%Flavor
Sirup Sorg	23.0	76.0	1.5
Sirup jgn	20.0	80.0	0.0
Sirup-semi	40.0	60.0	1.0
Campuran	25.0	75.0	1.0

- Input - output = akumulasi

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Contoh Soal Neraca Massa2 (jawab i)

1. Gambar diagram proses



2. Identifikasi sistem

3. Gunakan simbol-simbol :
- S** jumlah (kg) sirup sorgum murni
 - C** jumlah (kg) sirup jagung
 - P** jumlah (kg) sirup semi

4. Tulis persamaan yang dihasilkan :

Diperlukan 3 pers neraca bahan; yaitu gula, flavor & total massa

$$\begin{array}{lll}
 \text{Total} & : & S + C + P = 100 \quad \dots\dots\dots (1) \\
 \text{Gula} & : & 0.76 S + 0.8 C + 0.6 P = 0.75 \times 100 = 75 \quad \dots\dots\dots (2) \\
 \text{Flavor} & : & 0.015 S + 0 C + 0.01 P = 0.01 \times 100 = 1 \quad \dots\dots\dots (3)
 \end{array}$$

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Contoh Soal Neraca Massa2 (jawab ii)

$$\begin{array}{lcl} \text{Total} & : & S + C + P = 100 \quad \text{..... (1)} \\ \text{Gula} & : & 0.76 S + 0.8 C + 0.6 P = 0.75 \times 100 = 75 \quad \text{..... (2)} \\ \text{Flavor} & : & 0.015 S + 0 C + 0.01 P = 0.01 \times 100 = 1 \quad \text{..... (3)} \end{array}$$

5. Pecahkan persamaan yang diperoleh

Pecahkan P pada pers (3) sebagai fungsi S :

$$P = 100 - 1.5 S$$

- Substitusi nilai P dalam pers (1) :

$$S + C + 100 - 1.5 S = 100 \quad \text{.....} \rightarrow \text{jadi, } C = 0.5 S$$

- Substitusi nilai C dan P dalam pers (2) :

$$0.76 S + 0.8(0.5 S) + 0.6(100 - 1.5 S) = 75$$

$$0.26 S = 15; \quad \text{.....} \rightarrow \text{jadi, } S = 57.69$$

- Pecahkan nilai C dan P :

$$C = 0.5 S = 0.5 (57.69) = 28.85$$

$$P = 100 - 1.5 S = 100 - 1.5(57.69) = 13.46$$

- Jadi, campuran itu adalah :

$$S + C + P = 57.69 + 28.85 + 13.46 = 100$$

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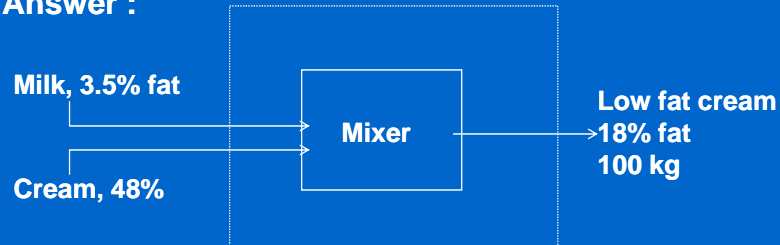
Example

Production of low fat cream (18% fat, w/w), from double cream (48% fat, w/w) and milk (3.5%, w/w).

How much double cream and milk are required to produce 100 kg low fat cream?

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Answer :



Let the required double cream = y kg and milk = x kg

Total mass balance equation :

$$y + x = 100 \text{ kg} \quad \dots\dots\dots \text{Eq.1}$$

The componen balance on the fat :

$$0.035x + 0.48y = 100(0.18) \quad \dots\dots\dots \text{Eq.2}$$

$$\text{Eq. 1 and 2 :} \quad 0.035(100-y) + 0.48y = 18$$

$$3.5 - 0.035y + 0.48y = 18$$

$$y = 32.58 \text{ kg}$$

$$\text{jadi} \quad \dots\dots\dots \quad X = 67.42 \text{ kg}$$

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Mass Balance Example 3

DO IT!

A fruit puree is dried in a continuous flow dehydrator.

The wet puree contains 0.80 $\text{H}_2\text{O}/\text{kg}$ puree while the dried puree contains 0.20 $\text{kg H}_2\text{O}/\text{kg}$ puree.

Flow rates of wet puree entering the dehydrator is 100 kg/h while dry puree leaving the dehydrator is 25 kg/h .

Heated drying air flows opposite to flow of the puree.

Moisture content of drying air entering and leaving the drier are 0.01 and 0.02 $\text{kg H}_2\text{O}/\text{kg}$, respectively.

What is the flow rate of drying air?

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Mass Balance Example 3 Answer (i)

Step 1. Draw a sketch or diagram describing process



Step 2. Identify boundaries of system with dotted lines

Input : puree in (0.80 H₂O/kg puree), at 100 kg/h
 drying air in (0.01 kg H₂O/kg)

Output : dried puree (0.20 kg H₂O/kg puree), at 25 kg/h
 drying air out (0.02 kg H₂O/kg)

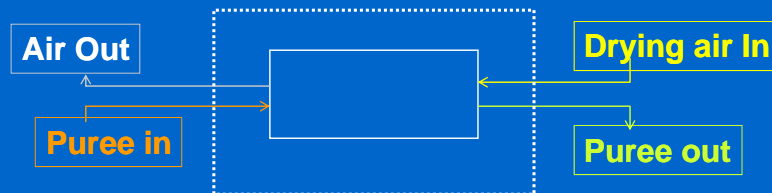
Step 3. Use symbols or letters to identify unknown items/quantities

- Let X kg/h represent the flow rate of drying air?

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Mass Balance Example 3 Answer (ii)

Step 4. Write mass balance equation



Balance for water : Water_{IN} = Water_{OUT}
 Basis : 1 h

$x \text{ kg DA (0.01 kg H}_2\text{O /kg DA) + 100 kg puree (0.8kg H}_2\text{O /kg puree) =}$
 $x \text{ kg DA (0.02 kg H}_2\text{O /kg DA) + 25 kg puree (0.2 kg H}_2\text{O/kg puree)}$

$0.01x + 80 = 0.02x + 5$
 $x = 75/0.01 = 7500$

Flow rate of drying air = 7500 kg/h

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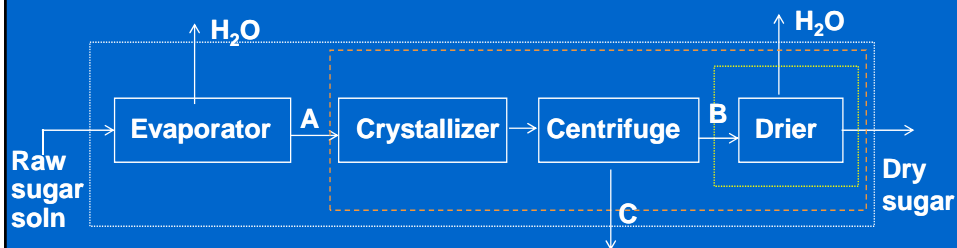
MATERIAL BALANCE FOR COMPLEX PROCESSING

Example of sugar crystallization

- Determine the amount of sugar that can be produced from 100,kg of sugar solution containing 20% (w/w) sugar, 1% (w/w) water soluble (uncrystallizable) impurity.
- The process are as the following :
- Solution is concentrated to 75% sugar, cooled to 20°C, and centrifuged, and the crystals are then dried.

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1. Diagram



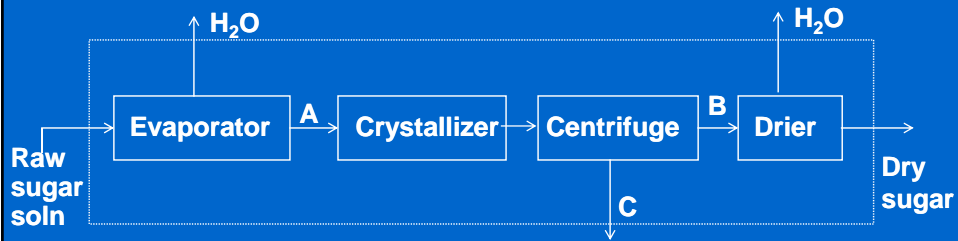
A : concentrated sugar soln (75% sugar,w/w)

B : wet sugar crystal

C : low concentration sugar soln

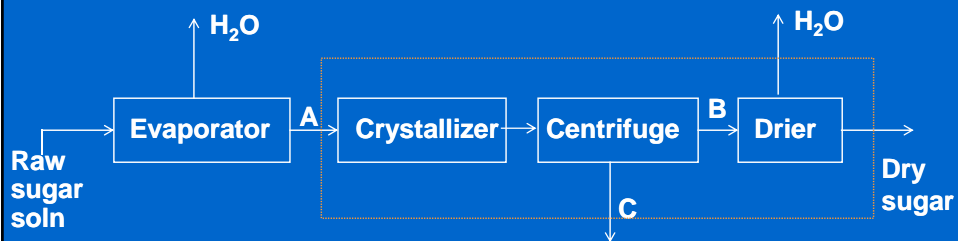
2. Identify system?

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System a :

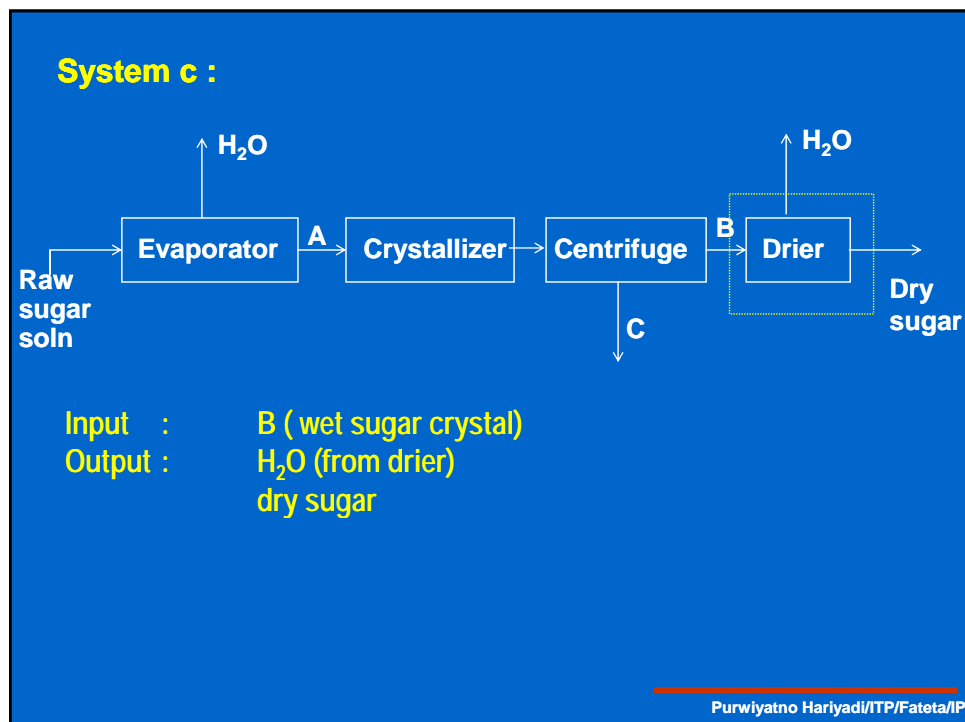
Input : raw sugar soln
 Output : H₂O (from evaporator)
 H₂O (from drier)
 C : low concentration sugar soln
 dry sugar

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System b :

Input : concentrated sugar soln (75% sugar,w/w)
 Output : H₂O (from drier)
 C : low concentration sugar soln
 dry sugar

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MASS BALANCE EXAMPLE 4.

- Crystallization of 100 kg of a concentrated sugar soln (85% sugar and 1 % inert, water soluble impurities).
- After cooling (crystallization), mixture was then centrifuged to separate crystal and a liquid fraction (mother liquor).
- Mother liquor contain 60% sucrose (w/w). Crystals slurry contain 20% (w/w) mother liquor.
- Do mass balance analysis for the process!

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MASS BALANCE EXAMPLE 4.....answer (i)

1. Diagram

2. Identify system

Input : Conc. Sugar soln
(100 kg, 85% sucrose, 1% impurities, 14% water)

Output : Crystal slurry (20% mother liquor)
Mother liquor (60% sucrose)

3. Symbol :

let S = total mass of conc. Sugar soln
C = total mass of crystal produced
M = total mass of mother liquor produced

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MASS BALANCE EXAMPLE 4.....answer (ii)

4. Mass balance equations

Total mass balance :
 $S = C + M$ Eq. 1

Balance of sucrose :
 $0.85S = 0.6M + [0.8(C) + 0.2(C)0.6]$ Eq. 2

Balance of water :
let x = mass fraction impurities in mother liquor
 $0.14S = M (0.4-x) + C(0.2)(0.4-x)$ Eq. 3

Balance of Impurities :
 $0.01S = M(x) + 0.2C(x)$ Eq. 4

..... 3 unknown, 4 equation!!

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BASIS AND TIE MATERIAL

Basis of calculation :

- important if no initial quantities are given
- important for continuous process

Tie Material :

- Component used to relate the quantity of one process stream to the quantity of another
- Usually : component that does not change during process
 - * solid in dehydration process
 - * solid in evaporation process

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RECYCLING ?? Toledo p.77

Falling film evaporator, capacity 10 kg water/h.

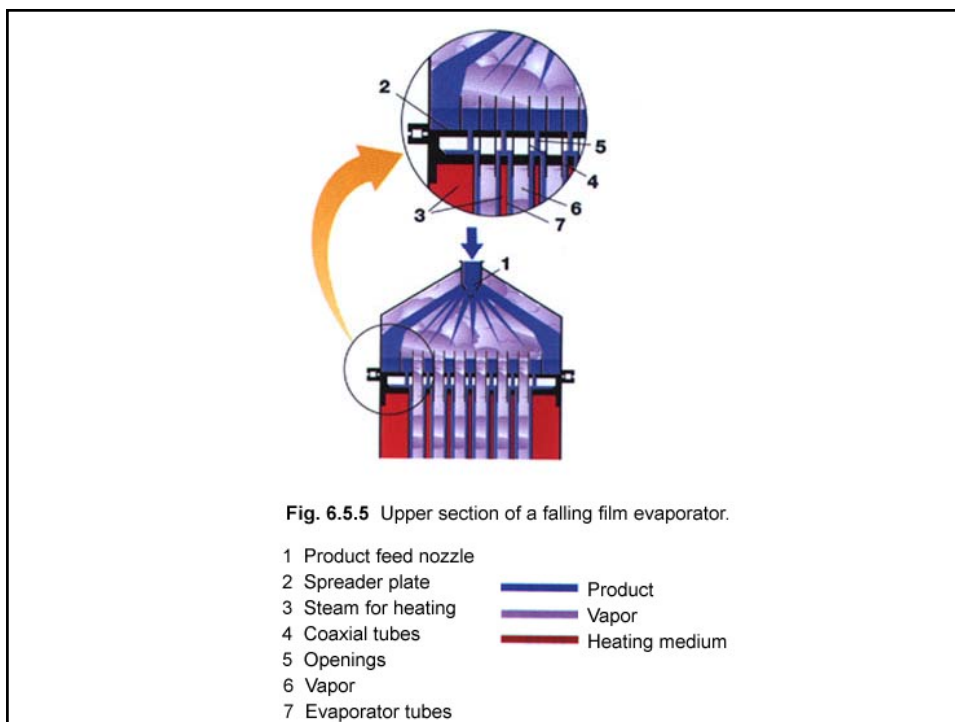
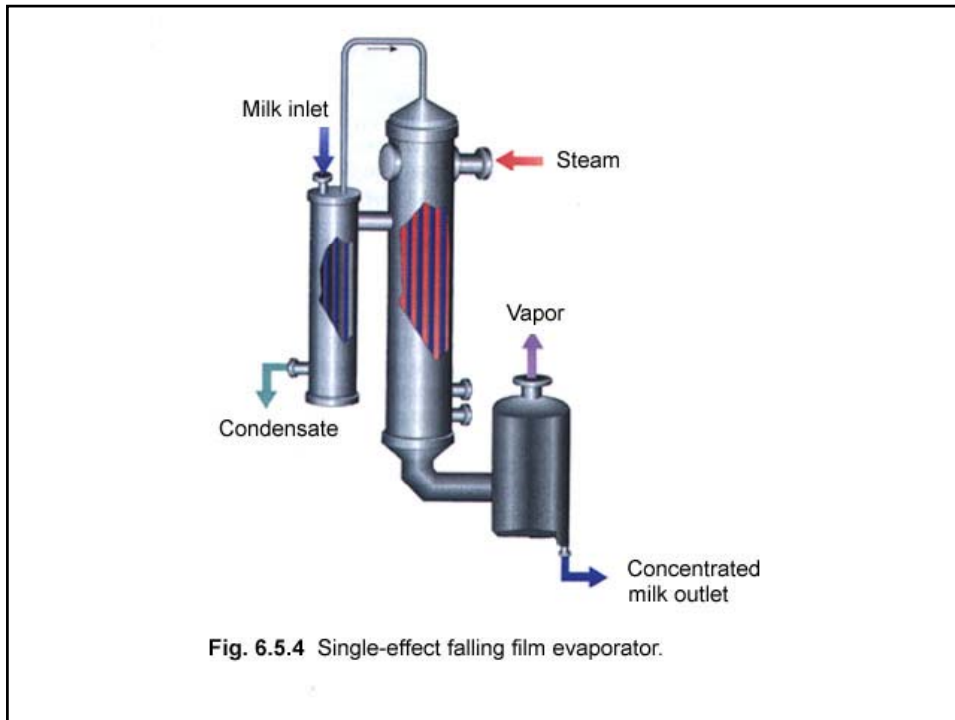
Feed enters at 5.5% solids and a 25% solid is desired.

To do that, system of recycling was used, at wich recycling pump moves 20 kg/h og fluid into the evaporator.

Calculate :

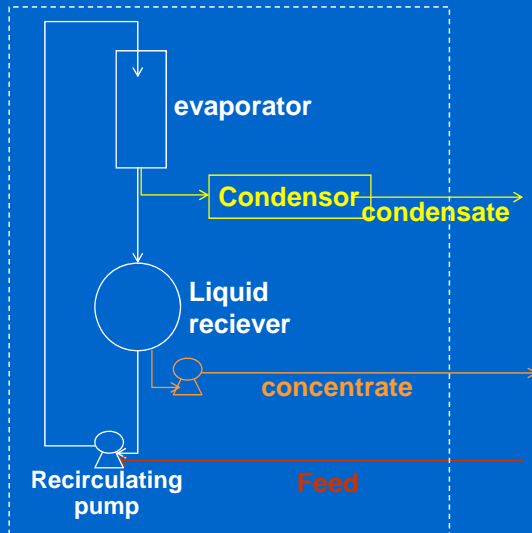
- a. the feed rate
- b. concentrate production rate
- c. amount of concentrate recycled
- d. concentration of mixture of feed and recycled concentrate

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RECYCLING ?? Toledo p.77 Answer (i)

1. Diagram?



1. Boundary of the system ?

Input :
Feed (5.5 % solids)

Output :
Condensate : 10 kg/h
Concentrate

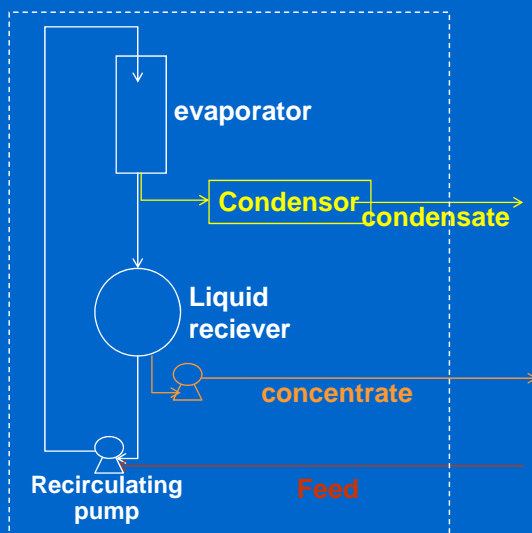
3. Symbols?

Feed rate = F
Condensate rate = $V=10$
Concentrate rate = C

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RECYCLING ?? Toledo p.77 Answer (ii)

4. Mass balance equation(s)



Total mass balance :
 $F = C + V = C + 10$ Eq.1

Balance of Solid :
 $0.055F = 0.25C$ Eq. 2

5. Solve the equations

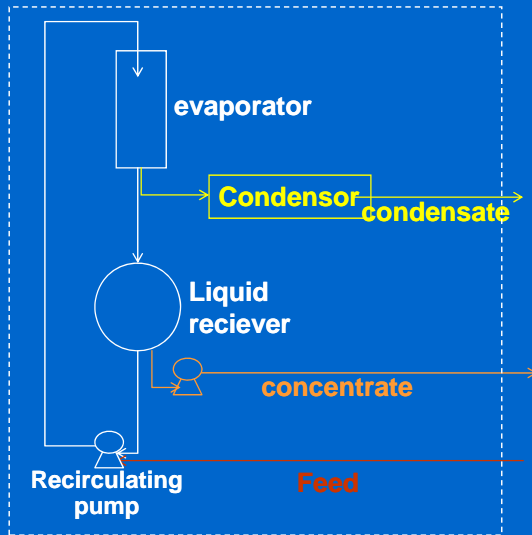
Eq.2. $F = (0.25/0.055)C$
 $F = 4.545C$ Eq.3

Eq.1 dan 3 :
 $4.545C = C + 10$
 $C = 10/3.545 = 2.52$

Jadi concentrate rate
= 2.52 kg/h

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RECYCLING ?? Toledo p.77 Answer (iii)



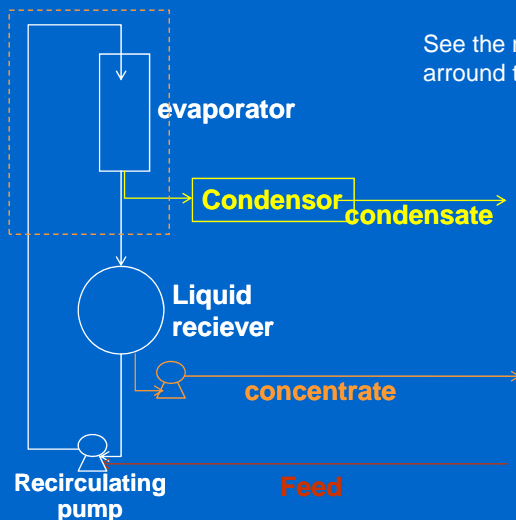
Back to eq.3.
 $F = 4.545C$
 $= 4.545(2.82)$
 $= 12.82$

Feed rate = 12.82 kg/h

To answer question c and d, we need to change the (boundary of) system analyzed

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RECYCLING ?? Toledo p.77 Answer (iv)



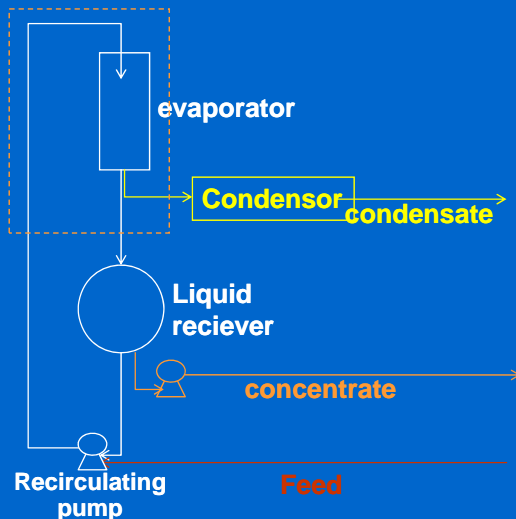
See the new system, around the evaporator

Input :
 Feed + Recycled
 (20 kg/h)

Output :
 Condensate
 $V = 10 \text{ kg/h}$
 Concentrate total
 (25% solid)

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RECYCLING ?? Toledo p.77 Answer (v)



Let total concentrate = C_t

Balance of total mass :
 $F + R = 20 = V + C_t$
 $12.82 + R = 20 = 10 + C_t$

$R = 7.18$
 (amount of concentrate recycled : 7.18 kg/h)

d. concentration of mixture of feed and recycled concentrate ? x

$C_t = 20 - 10 = 10$
 $x(20) = 10(0.25)$
 $x = 2.5/20 = 0.125$
 Concentration = 12.5%

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Material Balance for Blending Processes

- blending and proportioning is conducted to give products of desired composition
- optimization of composition with constraints on prices of raw materials is best solved by linear programming

Example

A processing plant is producing minced meat which must contain 15% of fat. If this is to be made up from boneless cow beef with 23% of fat and from boneless bull beef with 5% of fat, what are the proportions in which these should be mixed?